Material Models in Simulation-Part 3 - New viscosity models

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### Evaluation Parameters

- material property based parameters
- evaluate effects seen in the process
- understand and interpret simulation results
- compare materials
- develop criteria for selection based on desired processability

Properties of Evaluation Parameters

- easily available
- measures or estimates of actual effects
- must be considered along with other relevant parameters



Plastics may bave large shear this mine recipes







### nature of the 2nd order matrix

- temperatures
  - » Tmelt
  - » Tmelt+20
  - » Tmelt-20
- shear rates
  - » 100
  - » 1000
  - » 10000

Т	γ	η
Tmelt-20	1000	η1
Tmelt	100	<mark>ղ</mark> 2
Tmelt	1000	η3
Tmelt	10000	η4
Tmelt+20	100	η5
Tmelt+20	1000	η6



temperature sensitivity of viscosity

- TVH = ( ln  $\eta$ 3 - ln  $\eta$ 6 ) / 20

Т	γ	η
Tmelt-20	1000	η1
Tmelt	100	η2
Tmelt	1000	η3
Tmelt	10000	η4
Tmelt+20	100	η5
Tmelt+20	1000	η6



rules

**TV\* 1E+03 Datapoint Testing Services** 



shear sensitivity of viscosity

- defining a limited power-law index.

» SHB= (  $\ln \eta 3$  -  $\ln \eta 4$  ) / 2.303

Т	γ	η
Tmelt-20	1000	η1
Tmelt	100	η2
Tmelt	1000	η3
Tmelt	10000	η4
Tmelt+20	100	η <b>5</b>
Tmelt+20	1000	η6



- 0<SHB < 1

- large SHB = shear sensitive
- important exception:
  - » broad newtonian PC)



New models used in Moldflo

viscosity:

Cross Model

 $\eta = \frac{\eta_0}{1 + \left(\frac{\eta_0 \dot{\gamma}}{\tau^*}\right)^{(1-N)}}$  $\eta_0 = B \exp\left(\frac{T_b}{T}\right) \exp\left(\beta P\right)$  $\eta$  Viscosity (*Pa*.sec)  $\dot{\gamma}$  Shear Rate (sec<sup>-1</sup>) T Temperature (C) *P* Pressure (Pa) Unknowns:  $B, T_{\rm h}, \beta, \tau^*, N$ 



- B -no direct relevance
- measures η<sub>o</sub> when taken with Tb
- "zero shear viscosity normalized for temperature"

$$\eta_0 = B \exp\left(\frac{T_b}{T}\right)$$



- Tb -measures temperature sensitivity of viscosity
- rules
  - if Tb is large, material is highly sensitive
  - semi-crystalline
    - » Tb is small and relatively constant
  - amorphous
    - » Tb is larger and increases with temperature



- τ\* -critical transition stress for shear-thinning behavior
   rules
  - if  $\tau^*$  is large, wide Newtonian region
  - if  $\tau^*$  is small, narrow Newtonian region
  - τ\* is small for simple linear polymers
    » eg HDPE, LDPE, PP
  - τ\* is large for polymers with large side chains
     » eg. PC



- N measures shear thinning behavior
  - inverse of the power-law index
- rules for N
  - -0 < N < 1
  - small N = shear sensitive
  - important exception:
    - » fails if shear thinning region is not defined



# Assessment of the Cross Model

- easy model
  - terms have direct physical relevance
  - easy to assess and evaluate
- temperature sensitivity of viscosity is constant
  - cannot model temperature sensitivity for amorphous materials

## New models used in Moldflow

viscosity:Cross-WLF

 $\eta = \frac{\eta}{1 + \left(\frac{\eta_0 \dot{\gamma}}{r^*}\right)^{(1-N)}}$  $\eta_0 = D_1 \exp \left[ \frac{-A_1 (T - T^*)}{A_2 + (T - T^*)} \right]$  $T^* = D_2 + D_3 P$  $\eta$  Viscosity (*Pa*.sec)  $\dot{\gamma}$  Shear Rate (sec<sup>-1</sup>) T Temperature (C) P Pressure (Pa) Unknowns:  $D_1 D_2 D_3 A_1 A_2 \tau^* N$ **Datapoint Testing Services** 



- D1 -no direct relevance
- similar to B
- measures  $\eta_o$  when taken with WLF equation
- "zero shear viscosity normalized for temperature"

$$\eta_0 = D_1 \exp\left[\frac{-A_1(T-T^*)}{A_2 + (T-T^*)}\right]$$

Evaluation Parameter Cross-WLF Model

- D<sub>2</sub> a reference temperature
- theoretically, the temperature where  $\eta$  goes to  $\infty$
- typically D2=Tg, and  $\eta = 10^9$  Pa.s
- D<sub>3</sub> defines the pressure sensitivity of D<sub>2</sub>

$$T^* = D_2 + D_3 P$$



- A<sub>1</sub> & A<sub>2</sub> WLF parameters
- A<sub>1</sub> defines the temperature sensitivity of viscosity
- A<sub>2</sub> defines change in temperature sensitivity with temperature
- classical WLF parameters are
  - $A_1 = 40.1, A_2 = 51.6; \text{ if } D2 = Tg$
  - not always so for plastics

## New models used in Mold $\left[1 + \left(\frac{\eta_0 \dot{\gamma}}{\tau^*}\right)^2\right]^{\left(\frac{1-N}{2}\right)}$ viscosity: Carreau Model $\eta_0 = B \exp\left(\frac{T_b}{T}\right) \exp\left(\beta P\right)$

 $\eta_{0} = B \exp\left(\frac{T_{b}}{T}\right) \exp\left(\beta P\right)$   $\eta \text{ Viscosity } (Pa. \text{sec})$   $\dot{\gamma} \text{ Shear Rate } (\text{sec}^{-1})$  T Temperature (C) P Pressure (Pa) $\text{ Unknowns: } B, T_{b}, \beta, \tau^{*}, N$ 



- similar to Cross model
- terms have similar relevance
- Carreau Model will give sharper transitions from Newtonian to shear thinning region

If the data follows the model



If the data does not follow the model



### rheological data may not be complete

 complete data should contain Newtonian & shear thinning regions

Issues in data fittis

- data must show the right temperature sensitivity trends
- if not, model coefficients are indeterminate
- extrapolation will be dangerous



- not generalized; designed for polymers
- predict the expected trends for polymers
- incorporate both Newtonian and shear-thinning behavior
- do not work well if polymer does not follow expected trend (rare cases)



- predict a particular kind of behavior
- prevent inaccuracies in measured data from affecting the model
- safer to use
- model coefficients have useful interpretations
- are adaptable to master-curves

Conclusions

- we have a wider range of models for simulation
- each has its own benefits
- with new Moldflow formats, we can select the best model.
- model coefficients contain vital information
  - if properly understood, they will save you time and money
- see previous presentations (MUG '96 & MUG'97) for details on how to use evaluation parameters.